



# ***The effects of injecting hydrogen (renewable gases)***

***EASEE-gas GMOM 28 March 2018 - Budapest***

**marcogaz**  
TECHNICAL ASSOCIATION  
OF THE EUROPEAN NATURAL GAS INDUSTRY

**Jos Dehaeseleer**

*Secretary General*

# Storage of surplus of renewable energy

## Sharp growing of renewable power generation

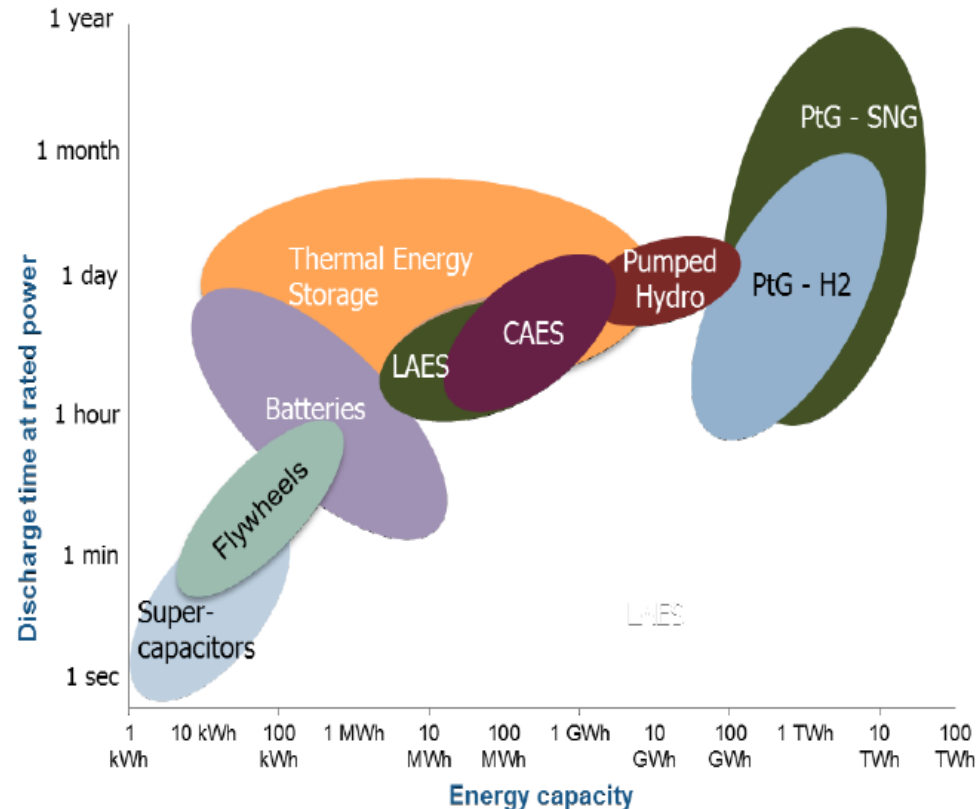
- *Peak power production generates curtailments*
- *Renewable power is intermittent*

## Need for power storage

## Different technologies available

- *Many of them under development*

## Hydrogen is an option



Source: World Energy Council, 2016

# Why hydrogen?

**Allow long term storage and transport of surplus of renewable energy**

**Hydrogen is an energy carrier**

**Different utilization options:**

- *Use in hydrogen application: heat, mobility, raw material, ...*
- *To transform in another fuel: methane, methanol, liquid fuels*
- *Injection into the natural gas network*

**Allow to use the large storage and transmission capacity of natural gas infrastructure**

**The natural gas infrastructures already exist and their capillarity along European territory allows connecting almost any production/utilization point**

**Natural gas infrastructure operators and associations are strongly committed to support the integration of renewable gases in their grids**

**Contribution to reduce the CO<sub>2</sub> footprint**

## Hydrogen main combustion properties vs natural gas (pipeline/LNG origin):

	Pipeline NG	LNG	H <sub>2</sub>
Hs (MJ/m <sup>3</sup> )	39.67	41.26	12.10
WI (MJ/m <sup>3</sup> )	50.73	52.35	45.88
Rel. Density	0.6114	0.6211	0.0696

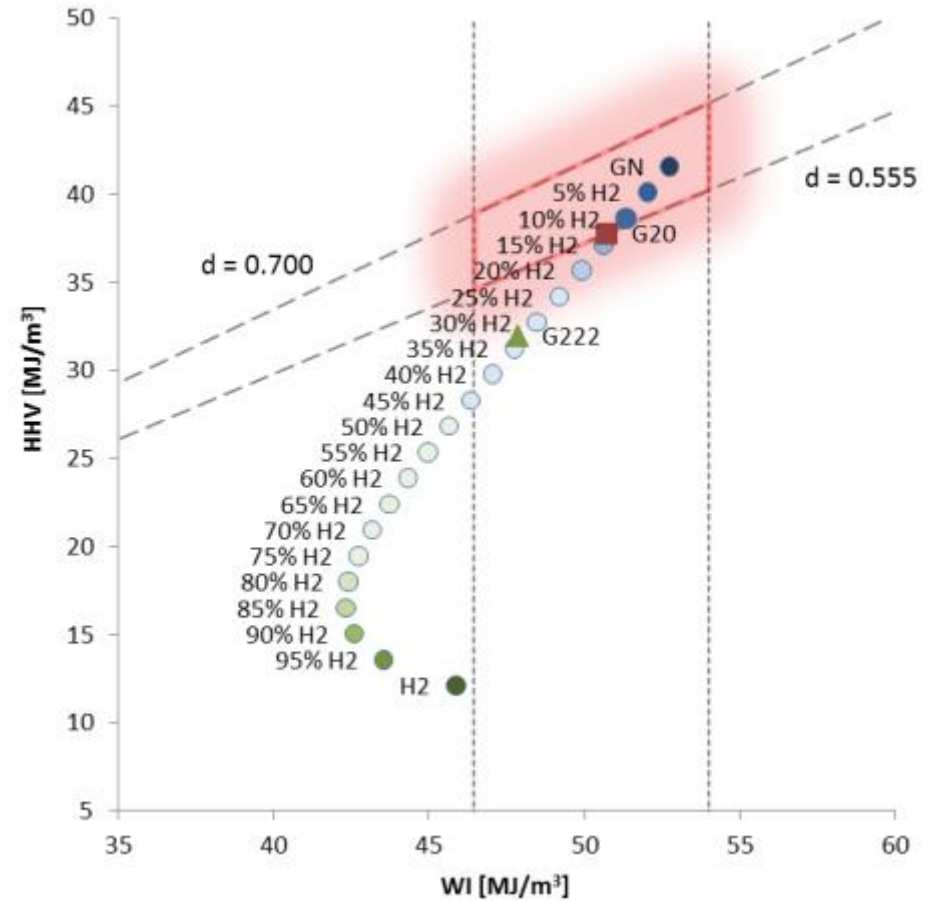
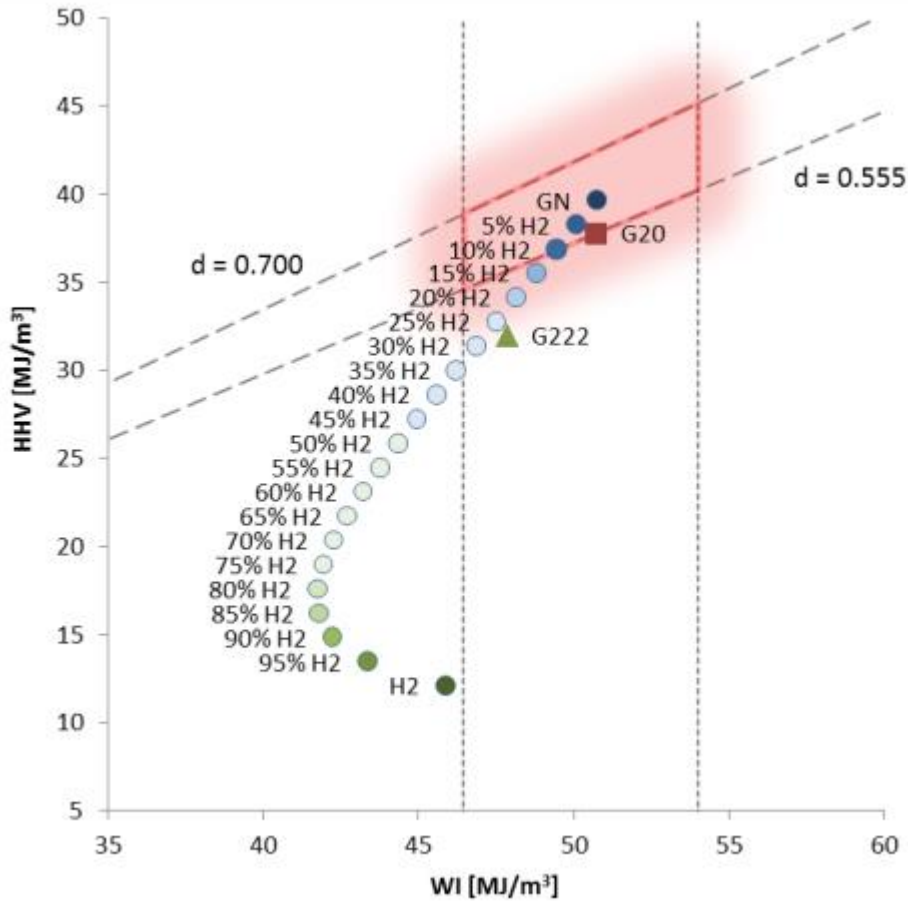
(15°C/15°C conditions)

- *Higher combustion velocity*
- *Higher flame temperature in stoichiometric combustion*

# Effect of adding hydrogen to natural gas

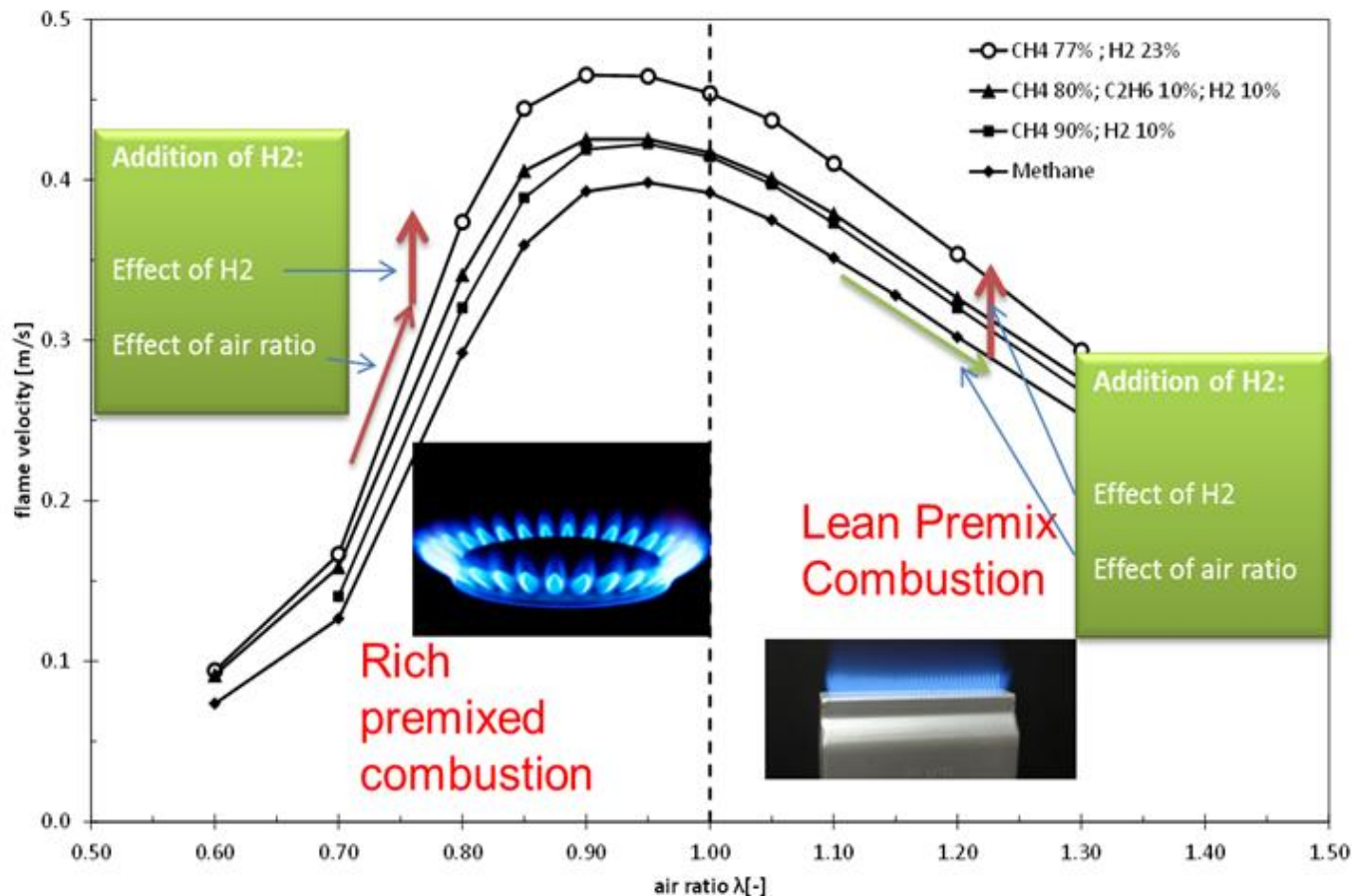
## Pipeline natural gas

## LNG



Red area: CBP natural gas specification limits as reference

# Effect on gas velocity of mixtures



Source: K. Altfeld & D. Pinchbeck (GERG),  
*Admissible Hydrogen Concentrations in Natural Gas Systems (HIPS The paper)*, 2013.

**Many gas applications are able to handle mixtures of natural gas and hydrogen without significant problems**

**Research has demonstrate that many residential and commercial appliances can handle up to 30 % hydrogen without safety concerns**

**Industrial application could handle up to 50 % hydrogen without negative impact if proper measurement and control technologies are applied**

**Gas turbines and gas engines are probably the most sensitive applications**

- *Manufacturers and researchers are investigating new technologies to address this*



### **Hydrogen reduces Wobbe index and calorific value of natural gas when mixed with it**

- *Reduction depends on natural gas composition*
- *Not only WI/GCV is affected*

### **Acceptable concentrations of hydrogen are different today for different end uses**

**Many consequences of hydrogen admixtures are qualitatively rather similar to gas natural fluctuations**

**Report MARCOGAZ - UTIL-GQ-17-29  
(<http://www.marcogaz.be/index.php/gas-utilization>)**

## **H<sub>2</sub> networks**

- *Leeds project (CCS)*

## **Mixtures NG/H<sub>2</sub>**

- *Note: city gas between 40 – 60% H<sub>2</sub>*
- *Rather stable WI/GCV needed for the appliances*
- *Depending on the materials/network structure*

## **Synthetic gases & biomethane**

- *Equivalent to Natural Gas*

## **Acceptable concentrations of hydrogen depending on the local situation**

- *Adaption of the network management*
- *Control/measurement*

## **If produced volume renewable gases (mixtures) > average Summer consumption:**

- *Cut-off (decrease injection)*
- *Storage (local, via transmission pipelines, UGS...)*

## **Investigation ongoing (MARCOGAZ/WELMEC/FARECOGAZ/CEN) on the use of conventional meters for the measurement of non conventional gases (including H<sub>2</sub> and H<sub>2</sub> mixtures)**

– *First conclusions:*

- *No problems expected for < 10% H<sub>2</sub> in NG*
- *> 10% H<sub>2</sub> : gas characteristics are progressively changed*

*Depending on the measuring principle investigation needed:*

- *Recalibration?*
- *Modification of the metrological model approvals*
- *The construction specifications of the pressurized parts, all gaskets/sealing and some components (sensors...) of the meters will need to be assessed for suitability, safety (tightness, embrittlement) and durability*
- *Static meters (US, Thermal mass, ...)*
- *Influence of the density, speed of sound, specific heat capacity...*

## Existing document : GI-EM-06-05

<http://www.marcogaz.be/index.php/gas-infrastructure2>

## New MARCOGAZ study started

- *describe and compare different methods that could be used to determine the attributed calorific value at each metering point when gases of different qualities and sources are entering at multiple points in the gas network (depending on the percentage of injection)*
  - *Assign a conventional CV (eventually after treating and/or blending)*
  - *Use tracking devices to monitor CV*
  - *Use of calculation methods*
  - *Measure CV at metering points*
  - *Examine the effects on the compressibility factor*
  - *...*
  - *Taking into account the different types of metering points used, residential, commercial, light industrial and industrial*

# Transmission network

Component	Knowledge is available	Gaps, needs further investigation
<b>Pipeline</b>	Degradation mechanisms Material and construction Process condition Effect H2% on crack propagation	For older pipelines a condition evaluation will be required. Existing defects should be evaluated because they can lead to lower percentages allowable H2.
<b>Welds</b>	Spec's for new to build 100%-H2 pipeline specify a hardness limit of ~250 Vickers (this is conservative in our opinion)	100%-Hydrogen cracking susceptibility at hardness > 250 Vickers (e.g, at 350 Vickers) Max allowable hardness for existing pipelines for 100% H2
<b>Compressor</b>	For reciprocating compressor: the gas used is only of limited importance Centrifugal compressors: performance depends on the density of the gas.	Compressor design should be in accordance with the gas composition.
<b>Gas turbines</b>	<1 % hydrogen addition is acceptable. Some new or upgraded types will be able to cope with concentrations up to 15 %	>1% Consequences for individual engines in installed base shall be investigated
<b>Valves</b>	Some parts might be not suitable for H2 Differential pressures Degradation non-metallic parts (e.g. gaskets)	Assess degradation non-metallic parts Investigate possible problems at differential pressures
<b>Safety pressure device</b>	No adverse effects expected, some parts might be not suitable for H2	Assess degradation non-metallic parts

# Storage (UGS)

INSTALLATION	PHENOMENA	TO CHECK
Surface facility	Corrosion	Integrity (idem for gas transport grid)
Compression units	Physical properties of H <sub>2</sub>	Efficiency and integrity (idem for gas transport grid)
Dehydration and desulfurization units	Physical properties of H <sub>2</sub>	Efficiency and integrity
Metering and gas quality monitoring	Physical properties of H <sub>2</sub>	For high % H <sub>2</sub> content (idem for gas transport grid)
Wells	Corrosion of steel, impact on elastomer sealing elements	Well integrity and containment
Reservoirs/caverns	Containment	Not different than Natural Gas
Reservoirs/caverns	Physical behaviour (dissolution, fingering)	Not drastically different than for Natural Gas
Reservoirs	Bio-chemical reaction	Potential reactions specific for each reservoir

# Safety

## Health of workers / end-users

- No known toxicological effects of H<sub>2</sub> on health (Source: SDS of H<sub>2</sub>)

## Gas detection

- Detectors to be recalibrated, adapted or replaced depending on the % of H<sub>2</sub> and depending of the type of detection system currently in place.

## ATEX Directive / zoning of installations

- Modification of current ATEX zones depending on the % of H<sub>2</sub>.
- Electrical installations could need adaptations or replacement above 15% of H<sub>2</sub>. (EN60079-10)

## Odorisation

- Impact of H<sub>2</sub> on the smell of the mixture to be assessed.

## Auto-ignition temperature

- Natural Gas (575...640°C) +/- the same as pure H<sub>2</sub> (560 °C).

## Combustion/Flame

- Different for H<sub>2</sub>



**Thank you !**

**marcogaz**

TECHNICAL ASSOCIATION  
OF THE EUROPEAN NATURAL GAS INDUSTRY

Avenue Palmerston 4  
1000 Brussels  
BELGIUM  
T: +32 2 237 11 39  
[www.marcogaz.org](http://www.marcogaz.org)